# An artificial-dissipation-based fractional step scheme for upper-convected Maxwell (UCM) fluid flow past a circular cylinder

# C.-B. Liu and P. Nithiarasu<sup>\*,†</sup>

School of Engineering, Swansea University, Swansea SA2 8PP, U.K.

## SUMMARY

The fully explicit characteristic-based split (CBS) scheme is employed to solve viscoelastic flow problems. The upper-convected Maxwell (UCM) model is employed in the present study. In addition to allowing equal-order interpolations for pressure and velocity, the proposed method along with an appropriate artificial damping scheme is able to produce stable solutions for different Deborah numbers (De). The higher-order time terms introduced by the simplified characteristic Galerkin approximation are sufficient to obtain stable solution at very low De, but an additional damping is essential to maintain positive definitiveness of the conformation tensor at higher De. We demonstrate the need for an additional damping by analysing the basic forward time central space scheme applied to the constitutive equations. A second-order artificial damping is employed to counteract the negative dissipation introduced by the explicit time discretization. The example studied in this paper is the widely used and difficult problem of flow past a circular cylinder. The results presented show that the velocity and extra stresses converge easily to a steady state at lower De values. At higher De values, the convergence to steady state is slow due to the incremental way in which the artificial damping is added. Copyright © 2008 John Wiley & Sons, Ltd.

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## 1. INTRODUCTION

The three major issues of current interest in the numerical modelling of viscoelastic flows are stability, large memory overhead and accuracy. Stability and accuracy are closely linked. The

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<sup>\*</sup>Correspondence to: P. Nithiarasu, School of Engineering, Swansea University, Swansea SA2 8PP, U.K. †E-mail: P.Nithiarasu@swansea.ac.uk

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memory overhead is the result of solving a number of extra stress component equations. The memory overhead can be reduced via matrix-free solution methods, such as the one used in the present study. The stability and accuracy of many numerical schemes deteriorate as the mesh is refined and the elasticity of the fluid is increased. There are a number of differential-type models available for representing a wide spectrum of viscoelastic fluids. Among the available models, the Oldroyd-B and upper-convected Maxwell (UCM) models are commonly employed and other models such as PTT and Giesekus are gaining popularity. In our previous publications [1, 2], we demonstrated how a matrix-free, artificial-compressibility-based fractional step method can be used to reduce some of the stability problems in using Oldroyd-B model. In addition to reducing instability, we have also demonstrated an improved accuracy of drag prediction by adding artificial damping [2]. A consistent second-order dissipation was used to maintain the positive definitiveness of the conformation tensor up to a Deborah number (*De*) of 2, although steady-state solution was obtained beyond De = 2. In the present work, we have extended the artificial-compressibility-based fractional step method to solve the more challenging UCM fluid model.

Owing to the lack of diffusion terms in the momentum equation, the UCM model is known to introduce severe stability problems as De is increased [3–7]. Many of the studies reported use structured meshes. In the present work, we have employed three fully unstructured meshes and one hybrid mesh to solve the UCM model for flow past a circular cylinder. However, one of the major objectives in viscoelastic flow calculations is to obtain accurate solutions at as high De as possible. Thus, any attempt that helps to push the De limit further on the fine meshes, without loosing positive definitiveness, should be investigated.

The method based on matrix-logarithm of conformation tensor for transforming constitutive equations has been recently proposed by Fattal and Kupferman [8]. The objective of this method is to design an algorithm that retains positive definitiveness of the conformation tensor and removes the growth of exponential stress profiles at higher Weissenberg numbers. Such a scheme was implemented using the finite element method by Hulsen [9] for viscoelastic flow past a confined circular cylinder using the Oldroyd-B model. Hulsen [9] introduced an extra differential equation to produce a symmetric matrix in the discrete elastic viscous split stress (DEVSS) formulation. An alternative form of logarithm-based method for solving all the governing equations was implemented with DEVSS-TG/SUPG up to a Deborah number of 0.7 [10]. Although the positive definiteness is guaranteed, the accuracy is not always assured [10]. In addition to extra variables, the matrix-logarithm-based method has been demonstrated only on the structured meshes. In the present study, the focus is either unstructured or hybrid mesh.

The stabilization proposed here is different from the classical methods such as SUPG [3, 4, 11, 12] and GLS [5, 13-16]. We use the time-stepping-based stabilization to reduce oscillations due to the Galerkin discretization of first-order terms [17-19]. In addition, we also employ a fractional step to reduce pressure instability (LBB condition) and an artificial compressibility scheme to keep the scheme matrix free [20-26]. This method is referred to as the characteristic-based split (CBS) method and it was employed to tackle Oldroyd-B fluid in References [1, 2].

Although the CBS scheme is conditionally stable for Newtonian fluids [19], the same conditional stability is not valid for differential equations governing the extra stresses of the viscoelastic fluids. This is demonstrated by analysing a simple time discretization of the constitutive equations later. Although the characteristic Galerkin (CG) scheme neutralizes some of the opposite stabilization terms, the simple time discretization used here retains some other negative diffusion terms. To counteract these negative diffusion terms, we may need additional dissipation. We have introduced

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a second-order, positive, additional damping to reduce the influence of these negative diffusion terms [1, 27–30].

In summary, the objective of the present work is to model UCM fluid past a circular cylinder using the CBS scheme and a novel artificial damping method. Section 2 summarizes the governing equations for the UCM model. In Section 3, the CBS scheme, the forward time central space (FTCS) scheme and the artificial dissipation (AD) method are discussed. Numerical solutions obtained for different *De*'s are given in Section 4. Some conclusions are derived in Section 5.

#### 2. MATHEMATICAL FORMULATIONS

The non-dimensional, isothermal equations for viscoelastic flows can be expressed as

$$\frac{\partial \mathbf{W}}{\partial t} + \frac{\partial \mathbf{F}_j}{\partial x_j} + \frac{\partial \mathbf{G}_j}{\partial x_j} = 0 \tag{1}$$

where

$$\mathbf{W} = \begin{bmatrix} \rho \\ \rho u_1 \\ \rho u_2 \end{bmatrix}, \quad \mathbf{F}_j = \begin{bmatrix} \rho u_j \\ \frac{1}{Re}(\delta_{1j}p) + \rho u_1 u_j \\ \frac{1}{Re}(\delta_{2j}p) + \rho u_2 u_j \end{bmatrix}, \quad \mathbf{G}_j = \begin{bmatrix} 0 \\ \frac{1}{Re}(-\tau_{1j}^n - \tau_{1j}^p) \\ \frac{1}{Re}(-\tau_{2j}^n - \tau_{2j}^p) \end{bmatrix}$$
(2)

in which the Newtonian deviatoric stress tensor can be expressed as

$$\tau_{ij}^{n} = (1 - \alpha) \left( \frac{\partial u_{i}}{\partial x_{j}} + \frac{\partial u_{j}}{\partial x_{i}} - \frac{2}{3} \frac{\partial u_{k}}{\partial x_{k}} \delta_{ij} \right)$$
(3)

and the non-Newtonian deviatoric stress tensor  $(\tau_{ij}^p = \tau_{ij}^e + \tau_{ij}^v)$ , which is given by the constitutive equation of extra stress for polymer contribution, can be expressed as

$$\tau_{ij}^{e} = -De\left[\frac{\partial \tau_{ij}^{p}}{\partial t} + \frac{\partial}{\partial x_{k}}(u_{k}\tau_{ij}^{p}) - \tau_{ik}^{p}\frac{\partial u_{j}}{\partial x_{k}} - \tau_{jk}^{p}\frac{\partial u_{i}}{\partial x_{k}}\right]$$
(4)

and

$$\tau_{ij}^{\nu} = \alpha \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} - \frac{2}{3} \frac{\partial u_k}{\partial x_k} \delta_{ij} \right)$$
(5)

In the above governing equations, p is the pressure,  $\rho$  is the density,  $u_j$  are the velocity components,  $\delta_{ij}$  is the Kronecker delta,  $\tau_{ij}^e$  is the polymer-contributed elastic stress,  $\tau_{ij}^v$  is the polymer-contributed viscous stress,  $\alpha = \eta_{m0}/\eta_0$  in which  $\eta_{m0}$  represents the polymer-contributed viscosity and  $\eta_0$  represents the zero shear rate viscosity, Re is the Reynolds number and De is the Deborah number defined as

$$Re = \frac{\rho_{\infty} u_{\infty} L}{\eta_0}, \quad De = \frac{\lambda u_{\infty}}{L} \tag{6}$$

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where subscript  $\infty$  indicates a free stream value, *L* is a characteristic length indicating the radius of a circular cylinder,  $\lambda$  is the relaxation time and  $\eta_0 = \eta_n + \eta_{m0}$  in which  $\eta_n$  represents the Newtonian dynamic viscosity. In Equation (4), when  $0 < \alpha < 1$ , the constitutive equation describes the Oldroyd-B model and the UCM model is obtained when  $\alpha = 1$ .

## 3. NUMERICAL FORMULATIONS

## 3.1. CBS scheme

The CBS scheme is based on the simplified CG procedure and a fractional step method [17-19]. In this paper, a fully explicit CBS form [1, 2, 20, 21] has been employed to solve Maxwell fluid flow past a circular cylinder. Following the intermediate momentum at the first step, the pressure is calculated from the modified mass conservation at step 2. The velocity field is corrected at step 3. Finally, the discretized constitutive equations are solved with CG stabilization terms at the fourth step. The first three steps are standard and are available in previously published articles [18, 20-26]. Only the discrete forms of the constitutive equation are discussed here. The semi-discrete form of step 4 is

$$\begin{aligned} \Delta \tau_{ij}^{p} &= \tau_{ij}^{p^{n+1}} - \tau_{ij}^{p^{n}} \\ &= \Delta t \left[ -\frac{\partial}{\partial x_{k}} (u_{k} \tau_{ij}^{p}) - \frac{\tau_{ij}^{p}}{De} \right]^{n} \\ &+ \Delta t \left[ \tau_{ik}^{p} \frac{\partial u_{j}}{\partial x_{k}} + \tau_{jk}^{p} \frac{\partial u_{i}}{\partial x_{k}} + \frac{\alpha}{De} \left( \frac{\partial u_{i}}{\partial x_{j}} + \frac{\partial u_{j}}{\partial x_{i}} - \frac{2}{3} \frac{\partial u_{k}}{\partial u_{k}} \delta_{ij} \right) \right]^{n} \\ &+ \frac{(\Delta t)^{2}}{2} \left\{ u_{m} \frac{\partial}{\partial x_{m}} \left[ \frac{\partial}{\partial x_{k}} (u_{k} \tau_{ij}^{p}) + \frac{\tau_{ij}^{p}}{De} \right] \right\}^{n} \\ &+ \frac{(\Delta t)^{2}}{2} \left\{ u_{m} \frac{\partial}{\partial x_{m}} \left[ - \left( \tau_{ik}^{p} \frac{\partial u_{j}}{\partial x_{k}} + \tau_{jk}^{p} \frac{\partial u_{i}}{\partial x_{k}} \right) \right] \right\}^{n} \\ &+ \frac{(\Delta t)^{2}}{2} \left\{ u_{m} \frac{\partial}{\partial x_{m}} \left[ - \frac{\alpha}{De} \left( \frac{\partial u_{i}}{\partial x_{j}} + \frac{\partial u_{j}}{\partial x_{i}} - \frac{2}{3} \frac{\partial u_{k}}{\partial u_{k}} \delta_{ij} \right) \right] \right\}^{n} \end{aligned}$$
(7)

In the above equation, the higher-order terms act as a convection-stabilizing mechanism. The CG procedure gives the positive diffusion, which may be expressed in compact form as

$$D_{ij}^{+} = \frac{\Delta t}{2} \left[ u_m \frac{\partial}{\partial x_m} \left( -\frac{\partial \tau_{ij}^p}{\partial t} \right) \right]^n \tag{8}$$

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where the time rate of increasing extra stress is

$$\frac{\partial \tau_{ij}^{p}}{\partial t} = -\frac{\partial}{\partial x_{k}} (u_{k} \tau_{ij}^{p}) + \tau_{ik}^{p} \frac{\partial u_{j}}{\partial x_{k}} + \tau_{jk}^{p} \frac{\partial u_{i}}{\partial x_{k}} - \frac{\tau_{ij}^{p}}{De} + \frac{\alpha}{De} \left( \frac{\partial u_{i}}{\partial x_{j}} + \frac{\partial u_{j}}{\partial x_{i}} - \frac{2}{3} \frac{\partial u_{k}}{\partial x_{k}} \delta_{ij} \right)$$
(9)

and for the two-dimensional viscoelastic flow problems, we have this in detailed form for each component of the constitutive equation as

$$D_{11}^{+} = -\frac{\Delta t}{2} \left[ u_1 \frac{\partial}{\partial x_1} \left( \frac{\partial \tau_{11}^p}{\partial t} \right) + u_2 \frac{\partial}{\partial x_2} \left( \frac{\partial \tau_{11}^p}{\partial t} \right) \right]^n$$

$$D_{12}^{+} = D_{21}^{+} = -\frac{\Delta t}{2} \left[ u_1 \frac{\partial}{\partial x_1} \left( \frac{\partial \tau_{12}^p}{\partial t} \right) + u_2 \frac{\partial}{\partial x_2} \left( \frac{\partial \tau_{12}^p}{\partial t} \right) \right]^n$$

$$D_{22}^{+} = -\frac{\Delta t}{2} \left[ u_1 \frac{\partial}{\partial x_1} \left( \frac{\partial \tau_{22}^p}{\partial t} \right) + u_2 \frac{\partial}{\partial x_2} \left( \frac{\partial \tau_{22}^p}{\partial t} \right) \right]^n$$
(10)

Applying the standard Galerkin approximation to the semi-discrete form of the equation (Equation 7), the final matrix form of the constitutive equations is obtained as

$$\Delta \underline{\tilde{\tau}}^{\tilde{p}} = -\mathbf{M}_{\tau^{p}}^{-1} \Delta t [(\mathbf{C}_{\tau^{p}} \underline{\tilde{\tau}}^{\tilde{p}} + \mathbf{K}_{\tau^{p}} \underline{\tilde{\tau}}^{\tilde{p}} - \mathbf{D}_{\tau^{p}}) - \Delta t (\mathbf{K}_{\mathbf{s}} \underline{\tilde{\tau}}^{\tilde{p}} + \mathbf{T}_{\mathbf{s}} \underline{\tilde{\tau}}^{\tilde{p}} - \mathbf{D}_{\mathbf{s}})]^{n}$$
(11)

where the extra stress variables are approximated using same-order interpolation functions as velocity and pressure. In the present study, we use linear triangular elements for the spatial discretization of all variables. The matrices in Equation (11) are given as

$$\begin{split} \mathbf{M}_{\tau^{p}} &= \int_{\Omega} \mathbf{N}_{\tau^{p}}^{\mathrm{T}} \mathbf{N}_{\tau^{p}} \, \mathrm{d}\Omega, \quad \mathbf{C}_{\tau^{p}} = \int_{\Omega} \mathbf{N}_{\tau^{p}}^{\mathrm{T}} (\nabla^{\mathrm{T}} (\mathbf{u} \mathbf{N}_{\tau^{p}})) \, \mathrm{d}\Omega, \quad \mathbf{K}_{\tau^{p}} = \frac{\mathbf{M}_{\tau^{p}}}{De} \\ \mathbf{D}_{\tau^{p}} &= \int_{\Omega} \mathbf{N}_{\tau^{p}}^{\mathrm{T}} \left( \underline{\tilde{\tau}}^{\tilde{p}} \nabla \mathbf{N}_{\mathbf{u}} \tilde{u} + \frac{\underline{\tilde{\tau}}^{\tilde{v}}}{De} \right) \mathrm{d}\Omega, \quad \mathbf{K}_{\mathbf{s}} = -\frac{1}{2} \int_{\Omega} (\nabla^{\mathrm{T}} (\mathbf{u} \mathbf{N}_{\tau^{p}}))^{\mathrm{T}} (\nabla^{\mathrm{T}} (\mathbf{u} \mathbf{N}_{\tau^{p}})) \, \mathrm{d}\Omega \\ \mathbf{T}_{\mathbf{s}} &= -\frac{1}{2De} \int_{\Omega} (\nabla^{\mathrm{T}} (\mathbf{u} \mathbf{N}_{\tau^{p}}))^{\mathrm{T}} \mathbf{N}_{\tau^{p}} \, \mathrm{d}\Omega \\ \mathbf{D}_{\mathbf{s}} &= -\frac{1}{2} \int_{\Omega} (\nabla^{\mathrm{T}} (\mathbf{u} \mathbf{N}_{\tau^{p}}))^{\mathrm{T}} \left( \underline{\tilde{\tau}}^{\tilde{p}} \nabla \mathbf{N}_{\mathbf{u}} \tilde{u} + \frac{\underline{\tilde{\tau}}^{\tilde{v}}}{De} \right) \mathrm{d}\Omega \end{split}$$
(12)

## 3.2. FTCS scheme

As the constitutive equations are substantially different from standard convection equations, explaining the negative diffusion generated may be easier using the FTCS scheme. To demonstrate the negative diffusion, the one-dimensional constitutive equation is discretized using the finite-difference-based FTCS scheme as

$$\frac{\tau_l^{p^{n+1}} - \tau_l^{p^n}}{\Delta t} + u_l^n \frac{\tau_{l+1}^{p^n} - \tau_{l-1}^{p^n}}{2\Delta x} - \tau_l^{p^n} \frac{u_{l+1}^n - u_{l-1}^n}{2\Delta x} + \frac{\tau_l^{p^n}}{De} - \frac{4\alpha}{3De} \frac{u_{l+1}^n - u_{l-1}^n}{2\Delta x} = 0$$
(13)

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Substituting the Taylor series expansion into Equation (13), we recover the differential form along with the following negative diffusion terms:

$$D_{l}^{-} = -\frac{\Delta t}{2!} \frac{\partial^{2} \tau_{l}^{p^{n}}}{\partial t^{2}} - \frac{(\Delta t)^{2}}{3!} \frac{\partial^{3} \tau_{l}^{p^{n}}}{\partial t^{3}} - \frac{(\Delta x)^{2}}{3!} \left[ u_{l}^{n} \frac{\partial^{3} \tau_{l}^{p^{n}}}{\partial x^{3}} - \left( \tau_{l}^{p^{n}} + \frac{4\alpha}{3De} \right) \frac{\partial^{3} u_{l}^{n}}{\partial x^{3}} \right] + O(\Delta t^{3})$$
(14)

Neglecting the third- and higher-order terms and generalizing to multi-dimensions, we obtain

$$D_{ij}^{-} = -\frac{\Delta t}{2!} \frac{\partial^2 \tau_{ij}^{p^n}}{\partial t^2}$$
(15)

For the two-dimensional problems, each component of approximate, negative diffusion may be expressed as (assuming a steady velocity field)

$$D_{11}^{-} = \frac{\Delta t}{2!} \left[ u_1 \frac{\partial}{\partial x_1} \left( \frac{\partial \tau_{11}^p}{\partial t} \right) + u_2 \frac{\partial}{\partial x_2} \left( \frac{\partial \tau_{11}^p}{\partial t} \right) \right]^n + \frac{\Delta t}{2!} \left[ \left( \frac{1}{De} - \frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} \right) \frac{\partial \tau_{11}^p}{\partial t} - 2 \frac{\partial \tau_{12}^p}{\partial t} \frac{\partial u_1}{\partial x_2} \right]^n + \frac{\Delta t}{2!} \left[ \frac{\partial \tau_{11}^p}{\partial x_1} \frac{\partial u_1}{\partial t} + \frac{\partial \tau_{11}^p}{\partial x_2} \frac{\partial u_2}{\partial t} - 2 \tau_{12}^p \frac{\partial}{\partial x_2} \left( \frac{\partial u_1}{\partial t} \right) \right]^n + \frac{\Delta t}{2!} \left[ \left( \tau_{11}^p + \frac{2\alpha}{3De} \right) \frac{\partial}{\partial x_2} \left( \frac{\partial u_2}{\partial t} \right) - \left( \tau_{11}^p + \frac{4\alpha}{3De} \right) \frac{\partial}{\partial x_1} \left( \frac{\partial u_1}{\partial t} \right) \right]^n$$
(16)

$$D_{12}^{-} = D_{21}^{-}$$

$$= \frac{\Delta t}{2!} \left[ u_1 \frac{\partial}{\partial x_1} \left( \frac{\partial \tau_{12}^p}{\partial t} \right) + u_2 \frac{\partial}{\partial x_2} \left( \frac{\partial \tau_{12}^p}{\partial t} \right) \right]^n$$

$$+ \frac{\Delta t}{2!} \left[ \frac{1}{De} \frac{\partial \tau_{12}^p}{\partial t} - \frac{\partial \tau_{11}^p}{\partial t} \frac{\partial u_2}{\partial x_1} - \frac{\partial \tau_{22}^p}{\partial t} \frac{\partial u_1}{\partial x_2} \right]^n$$

$$+ \frac{\Delta t}{2!} \left[ \frac{\partial \tau_{12}^p}{\partial x_1} \frac{\partial u_1}{\partial t} + \frac{\partial \tau_{12}^p}{\partial x_2} \frac{\partial u_2}{\partial t} \right]^n$$

$$+ \frac{\Delta t}{2!} \left[ - \left( \tau_{22}^p + \frac{\alpha}{De} \right) \frac{\partial}{\partial x_2} \left( \frac{\partial u_1}{\partial t} \right) - \left( \tau_{11}^p + \frac{\alpha}{De} \right) \frac{\partial}{\partial x_1} \left( \frac{\partial u_2}{\partial t} \right) \right]^n$$
(17)

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$$D_{22}^{-} = \frac{\Delta t}{2!} \left[ u_1 \frac{\partial}{\partial x_1} \left( \frac{\partial \tau_{22}^p}{\partial t} \right) + u_2 \frac{\partial}{\partial x_2} \left( \frac{\partial \tau_{22}^p}{\partial t} \right) \right]^n + \frac{\Delta t}{2!} \left[ \left( \frac{1}{De} - \frac{\partial u_2}{\partial x_2} + \frac{\partial u_1}{\partial x_1} \right) \frac{\partial \tau_{22}^p}{\partial t} - 2 \frac{\partial \tau_{21}^p}{\partial t} \frac{\partial u_2}{\partial x_1} \right]^n + \frac{\Delta t}{2!} \left[ \frac{\partial \tau_{22}^p}{\partial x_2} \frac{\partial u_2}{\partial t} + \frac{\partial \tau_{22}^p}{\partial x_1} \frac{\partial u_1}{\partial t} - 2 \tau_{21}^p \frac{\partial}{\partial x_1} \left( \frac{\partial u_2}{\partial t} \right) \right]^n + \frac{\Delta t}{2!} \left[ \left( \tau_{22}^p + \frac{2\alpha}{3De} \right) \frac{\partial}{\partial x_1} \left( \frac{\partial u_1}{\partial t} \right) - \left( \tau_{22}^p + \frac{4\alpha}{3De} \right) \frac{\partial}{\partial x_2} \left( \frac{\partial u_2}{\partial t} \right) \right]^n$$
(18)

Equations (16)–(18) show clearly that the first two terms of the negative diffusion are equal and opposite to the positive diffusion of the CG method as given in Equation (10). Thus, the CG method is expected to eliminate these two terms. However, the remainder of the negative diffusion terms are retained within the method. A careful investigation of these extra terms shows that some of them are zero (e.g. divergence-free velocity) and others are the function of De. This and our previous experiences with the Oldroyd-B model [2] show that inaccuracy and instability builds up as De increases. This effect of the negative diffusion may be reduced by employing two different approaches. The first is to add a positive diffusion exactly equal to the negative diffusion, which is retained by the scheme. Although sensible, this approach is extremely expensive due to the addition of many extra terms. The second approach is to add a consistent artificial damping term to the discrete constitutive equations to counteract the negative diffusion. This is a much cheaper approach than the former approach and is thus adopted in the present work. The following subsection gives two artificial damping options.

#### 3.3. AD method

It is well known that, in many situations, adding AD to a scheme can effectively damp the unstable phenomenon and smooth numerical results without destroying the accuracy. In this paper, artificial damping is added to the discrete constitutive equation (Equation (11)). Here, two different methods are proposed. The first dissipation method is based on the difference between consistent and lumped mass matrices, an approximation for second derivatives of the extra stress components [1, 27-30], i.e.

$$\frac{\partial}{\partial x_j} \left( h^2 \frac{\partial \tau_{ij}^p}{\partial x_j} \right) x_i \approx \mathbf{M}_{\tau^p}^{-1} (\mathbf{M}_{\tau^p} - \mathbf{M}_{\tau^p L}) \underline{\underline{\tau}}^{\tilde{p}}$$
(19)

With the addition of this artificial damping, the smoothed extra stress equation becomes

$$\Delta \underline{\tilde{\tau}}_{p}^{p} = \Delta \underline{\tilde{\tau}}_{p}^{p} + \Delta t \mathbf{M}_{\tau p}^{-1} \frac{C_{e} S_{e}}{\Delta t} (\mathbf{M}_{\tau p} - \mathbf{M}_{\tau p L}) \underline{\tilde{\tau}}_{p}^{p^{n}}$$
(20)

where subscript r indicates a smoothed solution, M is the mass matrix, subscript L indicates a lumped mass matrix and  $S_e$  is an elementally averaged switch of nodal pressure values,

given as

$$S_{i} = \frac{\left|\sum_{1}^{n} (p_{i} - p_{k})\right|}{\sum_{1}^{n} \left|p_{i} - p_{k}\right|}$$
(21)

where *n* is the number of nodes connected to *i*. In Equation (20),  $C_e$  is an artificial damping constant that should be carefully chosen to add an optimal amount of damping, sufficient to eliminate all negative eigenvalues of the conformation matrix within the flow domain. Equation (20) can also be visibly consistent with the original discretization of constitutive equation as the mesh is refined, which means that the element size *h* in Equation (19) tends to zero.

An alternative method [30] is to directly estimate the second derivative of extra stresses using the post-processed second derivatives of the extra stress components. The smoothed extra stress equation with this second option is

$$\Delta \underline{\tilde{\tau}}_{\underline{\tau}}^{p}{}_{r} = \Delta \underline{\tilde{\tau}}^{p}{}_{r} + \Delta t \mathbf{M}_{\tau p}{}^{-1} C_{e} h^{3} \frac{|\mathbf{u}| + \beta}{\bar{p}} |\nabla^{2} p|_{e} \mathbf{H}_{\tau p} \underline{\tilde{\tau}}^{p^{n}}$$
(22)

where  $\bar{p}$  is the average pressure, h is the local element size,  $\beta$  is the artificial wave speed and

$$\mathbf{H}_{\tau^p} = -\int_{\Omega} (\nabla \mathbf{N}_{\tau^p})^{\mathrm{T}} \nabla \mathbf{N}_{\tau^p} \,\mathrm{d}\Omega$$
<sup>(23)</sup>

In Equation (22), the second derivative of the extra stress is calculated at nodes using a postprocessing approach and the mean values are then calculated over each element [19]. In the present study, we present only the numerical results obtained from using the first artificial damping method due to its simplicity and cost effectiveness.

## 4. NUMERICAL EXAMPLE

#### 4.1. Domain and boundary conditions

As shown in Figure 1, a circular cylinder with radius R is placed into a rectangular channel at a distance 12R from the inlet. The channel is 28R long and the distance from the centre of the cylinder to the channel walls is 2R. The total height of the channel is 4R.

Three unstructured meshes and one hybrid mesh are generated with fine elements close to the cylinder surface. Typical element sizes on the cylinder surface are 0.10924, 0.05474, 0.00633 and 0.001, respectively, for the four different meshes generated. The hybrid mesh is automatically generated by growing normals on the cylinder surface. The surface normals are used as guides to place structured layers close to the cylinder surface [31]. The meshes in the vicinity of the cylinder are shown in Figure 2(a)–(d). Figure 3(a) and (b) shows two full grids (second and fourth grids) used in the study. From now onwards, we refer to the unstructured meshes as A, B and C with the finest being C and the coarsest being A. We refer to the fourth as mesh HD (hybrid Delaunay).

At the inlet and exit of the channel, parabolic velocity profiles are assumed, i.e.

$$u_1 = 1.5 \left( 1 - \frac{x_2^2}{4} \right) \tag{24}$$

$$u_2 = 0 \tag{25}$$

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Figure 1. Viscoelastic flow past a circular cylinder placed in a channel.

Consistent with the velocity boundary conditions, the steady distribution of extra stresses at the inlet section is assumed. The stress components are found by analytically solving the constitutive equations at the inlet. The non-dimensional form of the stress distribution at the inlet is given as

$$\tau_{11}^{p} = 2\alpha De \left(\frac{\partial u_1}{\partial x_2}\right)^2 \tag{26}$$

$$\tau_{12}^{p} = \alpha \frac{\partial u_{1}}{\partial x_{2}} \tag{27}$$

$$\tau_{22}^{p} = 0$$
 (28)

On the channel solid walls and cylinder surface, no slip conditions are assumed. No extra stress conditions are applied on channel walls and the cylinder surface. Both the viscoelastic fluid models are solved without the convection terms in the momentum equation.

## 4.2. Steady-state convergence criterion

The steady-state convergence criterion is fixed based on the normalized  $L_2$  norm of the residual of the equations. It is given as

$$\|e\|_{2}^{\phi} = \frac{\left[\sum_{i=1}^{m} (\|\phi\|_{i}^{n+1} - \|\phi\|_{i}^{n})^{2}\right]^{1/2}}{\left[\sum_{i=1}^{m} (\|\phi\|_{i}^{n+1})^{2}\right]^{1/2}}$$
(29)

where *m* is the number of nodes in the mesh,  $\phi$  indicates the second-order extra stress and velocity components. The above tolerance was reduced to a value of at least  $10^{-7}$ .

Some sample steady-state convergence histories of the UCM model results are shown in Figure 4. Figure 4(a) and (b) shows the convergence histories at De = 0.1 using mesh A. Figure 4(c) and (d) shows the convergence histories at De = 0.5 using mesh B. As seen, at De = 0.1, mesh A converged quickly to steady state. However, mesh B at De = 0.5 took substantially more number of time steps to reach steady state. To accelerate the solution to steady state, we use local time stepping methods



Figure 2. Viscoelastic fluid flow past a circular cylinder. (a) Mesh A (nodes: 13 977; elements: 27 267;  $\Delta d = 0.10924$ ); (b) mesh B (nodes: 16 690; elements: 32 617;  $\Delta d = 0.05474$ ); (c) mesh C (nodes: 33 189; elements: 64 759;  $\Delta d = 0.00633$ ); and (d) hybrid mesh HD (nodes: 35 506; elements: 69 918;  $\Delta d = 0.001$ ).



Figure 3. Viscoelastic flow past a circular cylinder. (a) Mesh B and (b) mesh HD.



Figure 4. Convergence history of the UCM model, Re = 0.0.

[1, 2]. At De = 0.1, the calculation took about 15 min to reach steady state on mesh A and took about 30 min on mesh HD using a standard PC (Intel Pentium 4 CPU 3.00 GHz and 1.00 GB of RAM 2.99 GHz). At highest De, for which the results are given, the calculation took about two days. This is due to the incremental variation of artificial damping introduced into the algorithm. We simply stopped calculations if a De value took substantially more time than two days.

## 4.3. Results

To maintain accuracy of the solution, the positive definiteness of the conformation matrix must be maintained throughout the computational field. The positive definiteness of the conformation matrix is also very important for the stability. This is done by making sure that the eigenvalues of the conformation tensor of additional stress are positive [32, 33]. The conformation tensor is given as

$$\tau_{ij}^A = \tau_{ij}^p + (\alpha/De)\delta_{ij} \tag{30}$$

Figure 5 shows eigenvalue contours of the additional stress tensors for the UCM model at De=0.7 using mesh HD. As seen, the additional dissipation has not only eliminated negative eigenvalues but also is crucial in obtaining a smooth solution.

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Figure 5. Eigenvalue distribution for the UCM model at De=0.7, Re=0.0 (mesh HD). (a)  $\lambda_1$  contours:  $\lambda_{1_{\min}}=1.432$ ,  $\lambda_{1_{\max}}=51.198$  and (b)  $\lambda_2$  contours:  $\lambda_{2_{\min}}=0.006$ ,  $\lambda_{2_{\max}}=3.817$ .

The drag force around the circular cylinder per unit length is calculated in non-dimensional form as

$$D = \int_{0}^{2\pi} [(-p + \tau_{11}^{n} + \tau_{11}^{p})\cos\theta + (\tau_{12}^{n} + \tau_{12}^{p})\sin\theta]R\,\mathrm{d}\theta$$
(31)

In the above equation, both the Newtonian viscous stress components  $\tau_{11}^n$  and  $\tau_{12}^n$  are zero for the Maxwell fluid employed.

The UCM model is obtained by choosing  $\alpha = 1$  in the constitutive equations. In all the cases presented, both in this and the following subsections, the steady-state solutions are first obtained without adding artificial damping. We then calculate the eigenvalues at all nodes of the domain. If we find any negative eigenvalue, we add additional damping and converge the solution to steady state. We incrementally increase the additional damping until all the negative eigenvalues are eliminated from the domain.

Figure 6(a) shows the mesh convergence studies carried out using all the four meshes. As seen, we were able to get good mesh convergence up to a Deborah number (*De*) of 0.7. Beyond this value, meshes C and HD took much longer to eliminate negative eigenvalues of the conformation tensor. Thus, we stopped calculations when the time needed for reaching steady state is substantially more than two days.

Figure 6(b) shows the total drag force distribution with respect to *De*. Both meshes A and B are easy to handle up to De = 0.6 due to a small number of negative eigenvalues appearing in the flow domain without the addition of the artificial damping. Eliminating the small number of negative eigenvalues is relatively easier compared with several hundreds of negative eigenvalues in the field. Beyond De = 0.6, the drag force produced by mesh A shows an upward trend. This may be the result of additional drag introduced by the artificial damping. When the element sizes are large, it is difficult to control the artificial damping. Larger element sizes, in general, mean larger artificial damping. This is the reason why the drag force produced by mesh A is deviating from its expected path. This shows that although the conformation matrix remains positive definite, the drag force is not necessarily accurate for a given mesh. Mesh B, on the other hand, only shows the effect of extra drag introduced to a much lesser extent. The drag force produced by mesh HD shows a consistent trend in line with other fine mesh results [5, 7]. At De = 0.7, mesh HD needed elimination of 335 negative eigenvalues around the cylinder. An AD constant value of  $C_e = 0.064$  is needed to make sure that all negative eigenvalues are removed. Beyond De = 0.7 the solution on

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Figure 6. Mesh convergence and drag force distribution for the UCM model. (a) Mesh convergence and (b) drag force distribution.

mesh HD is extremely slow to reach steady state. To eliminate hundreds of negative eigenvalues without jeopardizing the accuracy, we may need several incremental variations in the artificial damping constant. Although, in principle, this is possible, the cost of computation will be very high with an explicit scheme. It may be faster to get a solution on mesh HD with an implicit time discretization.

Table I provides a detailed comparison between the drag forces predicted using the CBS method and the other available methods. It appears that the CBS method closely agrees with the other methods.

To estimate the impact of the artificial damping on the results, we have plotted the extra stress  $\tau_{11}^p$  variation with and without artificial damping over the cylinder surface and along the midhorizontal line in Figure 7. The unstructured mesh A and a Deborah number of 0.3 are used for the comparison. As seen, steep changes in the stress are noted on the surface. The difference in the peak values of the stress with and without damping is apparent. The artificial damping clearly reduces the peak value. However, if the artificial damping is not used, the positive definiteness is

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De	Mesh A	Mesh B	Mesh C	Mesh HD	Fan <i>et al.</i> DEVSS	Miles <i>et al.</i> Mileo SMART
0.0	128.682	130.479	132.060	132.220	132.36	132.369
0.01	130.694	131.646	132.058	132.105		132.251
0.025						131.945
0.05	129.505	130.324	130.798	130.993		130.912
0.1	125.832	126.703	127.327	127.386	127.42	127.356
0.2	114.924	116.628		117.419	117.83	117.767
0.3	103.217	106.874		108.428	108.68	108.614
0.4	95.345	98.881	100.828	101.074	101.43	101.361
0.5	90.448	93.597		96.567	96.11	96.037
0.6	88.895	92.669		94.182	92.37	92.298
0.7	90.530	90.870		91.751	89.84	89.774
0.8	94.393	90.432			88.18	88.178
0.9		89.931				87.218
1.0		89.640				

Table I. Drag force calculated by the fully explicit CBS scheme for Maxwell fluid flow past a circular cylinder.



Figure 7. Extra stress  $\tau_{11}^p$  distribution over the cylinder and along the mid-vertical centerline, De=0.3 (mesh A). Comparison between the distributions with and without artificial damping.

not guaranteed. As given, there are four negative eigenvalues without damping ( $C_e = 0$ ). However, when a small amount of artificial damping is added ( $C_e = 5.5 \times 10^{-3}$ ), the negative eigenvalues disappear. It is also obvious that the influence of artificial damping on the stress value in the wake is negligibly small.

Figure 8 shows the extra stress  $\tau_{11}^p$  distribution over the cylinder and along the mid-horizontal line for different Deborah numbers using the hybrid mesh HD. The artificial damping is essential to eliminate negative eigenvalues beyond a Deborah number of 0.2. The stress profiles are much smoother than the ones obtained on Mesh A, demonstrating that the finer mesh produces a better solution. It is also noted that the peak value on the cylinder surface starts going down beyond



Figure 8. Extra stress  $\tau_{11}^p$  distribution over the cylinder and along the mid-vertical centerline for different Deborah numbers (mesh HD).

a Deborah number value of 0.5. This could be the effect of artificial damping. As the Deborah number increases, the demand for artificial damping also increases. The lower peak may be the result of controlled but incorrect artificial damping. Further theoretical research may be necessary to determine an optimal value of damping. A peak value change similar to the one on the cylinder surface is also noted in the wake. However, the peak value here goes down only beyond a Deborah number value of 0.6.

Often it is essential to check the qualitative results to make sure that the solution is smooth. In Figure 9 we show contours of the first normal stress difference  $N_1 = \tau_{11}^p - \tau_{22}^p$  and the two components of the extra stresses at De = 0.7. Mesh HD was used here to make sure that the solution is as accurate as possible. As seen the solution shows no unphysical oscillations in any part of the domain.

#### 5. CONCLUSIONS

In this paper the UCM model was studied using the fully explicit CBS scheme to solve viscoelastic flow over a stationary circular cylinder placed in a rectangular channel. An additional AD method was introduced into the discrete constitutive equations to counteract the negative dissipation. The artificial damping was essential in removing negative eigenvalues of the conformation matrix from the flow domain but AD is not always essential to reach steady state. The results were in close agreement with the published results at lower *De*, and at higher *De* values the deviation is small. In addition to demonstrating that the CBS scheme along with an artificial damping can be an alternative method to solve UCM equations, we have also demonstrated that the *De* limit can be further enhanced with the expense of substantially more computational time. However, a better way of carrying out higher *De* calculations may be via implicit treatment of the constitutive equations using appropriate methods. Implicit matrix-free methods such as GMRES may offer a faster option to solve the constitutive equations. Irrespective of the methods used, the artificial damping introduced will be useful in retaining the positive definitiveness of the problem.

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Figure 9. Maxwell fluid flow past a circular cylinder at De = 0.7, Re = 0.0 (mesh HD). (a)  $N_1$  contours:  $N_{1_{\text{min}}} = -12.458$ ,  $N_{1_{\text{max}}} = 48.517$ ; (b)  $\tau_{11}^p$  contours:  $\tau_{11_{\text{min}}}^p = -0.962$ ,  $\tau_{11_{\text{max}}}^p = 48.416$ ; and (c)  $\tau_{12}^p$  contours:  $\tau_{12_{\text{min}}}^p = -17.897$ ,  $\tau_{12_{\text{max}}}^p = 17.962$ .

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